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Static behaviour of natural gas and its flow in pipes

Ohirhian, P. U.

University of Benin, Petroleum Engineering Department, Benin City, Nigeria.

Email: peter@ohirhian.com, okuopet@yahoo.com

Abstract

A general differential equation that governs static and flow behavior of a compressible fluid in horizontal, uphill and downhill inclined pipes is developed. The equation is developed by the combination of Euler equation for the steady flow of any fluid, the Darcy-Weisbach formula for lost head during fluid flow in pipes, the equation of continuity and the Colebrook friction factor equation. The classical fourth order Runge-Kutta numerical algorithm is used to solve to the new differential equation. The numerical algorithm is first programmed and applied to a problem of uphill gas flow in a vertical well. The program calculates the flowing bottom hole pressure as 2544.8 psia while the Cullender and Smith method obtains 2544 psia for the 5700 ft (above perforations) deep well

Next, the Runge-Kutta solution is transformed to a formula that is suitable for hand calculation of the static or flowing bottom hole pressure of a gas well. The new formula gives close result to that from the computer program, in the case of a flowing gas well. In the static case, the new formula predicts a bottom hole pressure of 2640 psia for the 5790 ft (including perforations) deep well. Ikoku average temperature and deviation factor method obtains 2639 psia while the Cullender and Smith method obtains 2641 psia for the same well. The Runge-Kutta algorithm is also used to provide a formula for the direct calculation of the pressure drop during downhill gas flow in a pipe. Comparison of results from the formula with values from a fluid mechanics text book confirmed its accuracy. The direct computation formulas of this work are faster and less tedious than the current methods. They also permit large temperature gradients just as the Cullender and Smith method.

Finally, the direct pressure transverse formulas developed in this work are combined with the Reynolds number and the Colebrook friction factor equation to provide formulas for the direct calculation of the gas volumetric rate

Introduction

The main tasks that face Engineers and Scientists that deal with fluid behavior in pipes can be divided into two broad categories - the computation of flow rate and prediction of pressure at some section of the pipe. Whether in computation of flow rate, or in pressure transverse, the method employed is to solve the energy equation (Bernoulli equation for

liquid and Euler equation for compressible fluid), simultaneously with the equation of lost head during fluid flow, the Colebrook (1938) friction factor equation for fluid flow in pipes and the equation of continuity (conservation of mass / weight). For the case of a gas the equation of state for gases is also included to account for the variation of gas volume with pressure and temperature.

In the first part of this work, the Euler equation for the steady flow of any fluid in a pipe/conduit is combined with the Darcy - Weisbach equation for the lost head during fluid flow in pipes and the Colebrook friction factor equation. The combination yields a general differential equation applicable to any compressible fluid; in a static column, or flowing through a pipe. The pipe may be horizontal, inclined uphill or downhill.

The accuracy of the differential equation was ascertained by applying it to a problem of uphill gas flow in a vertical well. The problem came from the book of Ikoku (1984), "Natural Gas Production Engineering". The classical fourth order Runge-Kutta method was first of all programmed in FORTRAN to solve the differential equation. By use of the average temperature and gas deviation factor method, Ikoku obtained the flowing bottom hole pressure (P_{wf}) as 2543 psia for the 5700 ft well. The Cullender and Smith (1956) method

that allows wide variation of temperature gave a P_{wf} of 2544 psia. The computer program

obtains the flowing bottom hole pressure (P_{wf}) as 2544.8 psia. Ouyang and Aziz (1996) developed another average temperature and deviation method for the calculation of flow rate and pressure transverse in gas wells. The average temperature and gas deviation formulas cannot be used directly to obtain pressure transverse in gas wells. The Cullender and Smith method involves numerical integration and is long and tedious to use.

The next thing in this work was to use the Runge-Kutta method to generate formulas suitable for the direct calculation of the pressure transverse in a static gas column, and in uphill and downhill dipping pipes. The accuracy of the formula is tested by application to two problems from the book of Ikoku. The first problem was prediction of static bottom hole pressure (P_{ws}). The new formula gives a P_{ws} of 2640 psia for the 5790ft deep gas well. Ikoku average pressure and gas deviation factor method gives the

P_{ws} as 2639 psia, while the Cullender and Smith method gives the P_{ws} as 2641 psia. The second problem involves the calculation of flowing bottom hole pressure (P_{wf}). The new

formula gives the P_{wf} as 2545 psia while the average temperature and gas deviation factor of Ikoku gives the P_{wf} as 2543 psia. The Cullender and Smith method obtains a P_{wf} of 2544 psia. The downhill formula was first tested by its application to a slight modification of a problem from the book of Giles et al.(2009). There was a close agreement between exit pressure calculated by the formula and that from the text book. The formula is also used to calculate bottom hole pressure in a gas injection well.

The direct pressure transverse formulas developed in this work are also combined with the Reynolds number and the Colebrook friction factor equation to provide formulas for the direct calculation of the gas volumetric rate in uphill and downhill dipping pipes.

A differential equation for static behaviour of a compressible fluid and its flow in pipes

The Euler equation is generally accepted for the flow of a compressible fluid in a pipe. The equation from Giles et al. (2009) is:

$$\frac{dp}{\gamma} + \frac{v dv}{g} \pm d\ell \sin \theta + dh_1 = 0 \quad (1)$$

In equation (1), the plus sign (+) before $d\ell \sin \theta$ corresponds to the upward direction of the positive z coordinate and the minus sign (-) to the downward direction of the positive z coordinate.

The generally accepted equation for the loss of head in a pipe transporting a fluid is that of Darcy-Weisbach. The equation is:

$$H_L = \frac{f L v^2}{2gd} \quad (2)$$

The equation of continuity for compressible flow in a pipe is:

$$W = A \gamma v \quad (3)$$

Taking the first derivation of equation (3) and solving simultaneously with equation (1) and (2) we have after some simplifications,

$$\frac{dp}{d\ell} = - \frac{\left[\frac{f W^2}{2\gamma A^2 d g} \mp \gamma \sin \theta \right]}{\left[1 - \frac{W^2}{\gamma^2 A^2 g} \frac{d\gamma}{dp} \right]} \quad (4)$$

All equations used to derive equation (4) are generally accepted equations. No limiting assumptions were made during the combination of these equations. Thus, equation (4) is a general differential equation that governs static behavior compressible fluid flow in a pipe. The compressible fluid can be a liquid of constant compressibility, gas or combination of gas and liquid (multiphase flow).

By noting that the compressibility of a fluid (C_f) is:

$$C_f = \frac{1}{\gamma} \frac{d\gamma}{dp} \quad (5)$$

Equation (4) can be written as:

$$\frac{dp}{d\ell} = - \frac{\left[\frac{fW^2}{2\gamma A^2 dg} \mp \gamma \sin \theta \right]}{\left[1 - \frac{W^2 C_f}{\gamma A^2 g} \right]} \quad (6)$$

Equation (6) can be simplified further for a gas.
Multiply through equation (6) by γ , then

$$\frac{\gamma dp}{d\ell} = - \frac{\left[\frac{fW^2}{2gA^2 dg} \mp \gamma^2 \sin \theta \right]}{\left[1 - \frac{W^2 C_f}{\gamma A^2 g} \right]} \quad (7)$$

The equation of state for a non-ideal gas can be written as

$$\gamma = \frac{p M}{zRT} \quad (8)$$

Substitution of equation (8) into equation (7) and using the fact that

$$\frac{pdp}{d\ell} = \frac{1}{2} \frac{dp^2}{d\ell}, \text{ gives}$$

$$\frac{dp^2}{d\ell} = - \frac{\left[\frac{fW^2 zRT}{A^2 dMg} \mp \frac{2p^2 M \sin \theta}{zRT} \right]}{\left[1 - \frac{W^2 zRTC_f}{MA^2 g p} \right]} \quad (9)$$

The cross-sectional area (A) of a pipe is

$$A^2 = \left(\frac{\pi d^2}{4} \right)^2 = \frac{\pi^2 d^4}{16} \quad (10)$$

Then equation (9) becomes:

$$\frac{dP^2}{d\ell} = - \left[\frac{1.621139 \frac{fW^2 zRT}{d^5 M g} \mp \frac{2 M \sin \theta P^2}{zRT}}{1 - \frac{1.621139 W^2 zRT C_f}{M g d^4 P}} \right]. \quad (11)$$

The denominator of equation (11) accounts for the effect of the change in kinetic energy during fluid flow in pipes. The kinetic effect is small and can be neglected as pointed out by previous researchers such as Ikoku (1984) and Uoyang and Aziz(1996). Where the kinetic effect is to be evaluated, the compressibility of the gas (C_f) can be calculated as follows:

For an ideal gas such as air,

$$C_f = \frac{1}{p}. \text{ For a non ideal gas, } C_f = \frac{1}{p} - \frac{1}{z} \frac{\partial z}{\partial p}.$$

Matter et al. (1975) and Ohirhian (2008) have proposed equations for the calculation of the compressibility of hydrocarbon gases. For a sweet natural gas (natural gas that contains CO_2 as major contaminant), Ohirhian (2008) has expressed the compressibility of the real gas (C_f) as:

$$C_f = \frac{K}{p}$$

For Nigerian (sweet) natural gas $K = 1.0328$ when p is in psia

The denominator of equation (11) can then be written as

$$1 - \frac{KW^2 zRT}{M g d^4 P^2}, \text{ where } K = \text{constant.}$$

Then equation (11) can be written as

$$\frac{dy}{d\ell} = \frac{(A \pm By)}{\left(1 - \frac{G}{y}\right)} \quad (12)$$

where

$$y = p^2, \quad A = \frac{1.621139 f W^2 z R T}{g d^5 M}, \quad B = \frac{2 M \sin \theta}{z R T}, \quad G = \frac{K W^2 z R T}{g M d^4}.$$

The plus (+) sign in numerator of equation (12) is used for compressible uphill flow and the negative sign (-) is used for the compressible downhill flow. In both cases the z coordinate is taken positive upward. In equation (12) the pressure drop is $\sqrt{y_1 - y_2}$, with $y_1 > y_2$ and incremental length is $l_2 - l_1$. Flow occurs from point (1) to point (2). Uphill flow of gas occurs in gas transmission lines and flow from the foot of a gas well to the surface. The pressure at

the surface is usually known. Downhill flow of gas occurs in gas injection wells and gas transmission lines.

We shall illustrate the solution to the compressible flow equation by taking a problem involving an uphill flow of gas in a vertical gas well.

Computation of the variables in the gas differential equation

We need to discuss the computation of the variables that occur in the differential equation for gas before finding a suitable solution to it. The gas deviation factor (z) can be obtained from the chart of Standing and Katz (1942). The Standing and Katz chart has been curve fitted by many researchers. The version that was used in this section of the work that of Gopal(1977). The dimensionless friction factor in the compressible flow equation is a function of relative roughness (ϵ / d) and the Reynolds number (R_N). The Reynolds number is defined as:

$$R_N = \frac{\rho v d}{\mu} = \frac{W d}{A g \mu} \quad (13)$$

The Reynolds number can also be written in terms of the gas volumetric flow rate. Then

$$W = \gamma_b Q_b$$

Since the specific weight at base condition is:

$$\gamma_b = \frac{p_b M}{z_b T_b R} = \frac{28.97 G_g p_b}{z_b T_b R} \quad (14)$$

The Reynolds number can be written as:

$$R_N = \frac{36.88575 G_g P_b Q_b}{R g d \mu_g z_b T_b} \quad (15)$$

By use of a base pressure (p_b) = 14.7psia, base temperature (T_b) = 520°R and $R = 1545$

$$R_N = \frac{20071 Q_b G_g}{\mu_g d} \quad (16)$$

Where d is expressed in inches, $Q_b = \text{MMSCF} / \text{Day}$ and μ_g is in centipoises.

Ohirhian and Abu (2008) have presented a formula for the calculation of the viscosity of natural gas. The natural gas can contain impurities of CO_2 and H_2S . The formula is:

$$\mu_g = \frac{0.0109388 - 0.0088234xx - 0.00757210xx^2}{1.0 - 1.3633077xx - 0.0461989xx^2} \tag{17}$$

Where

$$xx = \frac{0.0059723p}{z \left(16.393443 - \frac{T}{p} \right)}$$

In equation (17) μ_g is expressed in centipoises(c p) , p in (psia) and Tin ($^{\circ}$ R)

The generally accepted equation for the calculation of the dimensionless friction factor (f) is that of Colebrook (1938). The equation is:

$$\frac{1}{\sqrt{f}} = -2 \log \left(\frac{\epsilon}{3.7d} + \frac{2.51}{R_N \sqrt{f}} \right) \tag{18}$$

The equation is non-linear and requires iterative solution. Several researchers have proposed equations for the direct calculation of f. The equation used in this work is that proposed by Ohirhian (2005). The equation is

$$f = \left[-2 \log \left(a - 2b \log (a + bx_1) \right) \right]^{-2} \tag{19}$$

Where

$$a = \frac{\epsilon}{3.7d}, \quad b = \frac{2.51}{R_N}$$

$$x_1 = -1.14 \log \left(\frac{\epsilon}{d} + 0.30558 \right) + 0.57 \log R_N (0.01772 \log R_N + 1.0693)$$

After evaluating the variables in the gas differential equation, a suitable numerical scheme can be used to it.

Solution to the gas differential equation for direct calculation of pressure transverse in static and uphill gas flow in pipes.

The classical fourth order Range Kutta method that allows large increment in the independent variable when used to solve a differential equation is used in this work. The solution by use of the Runge-Kutta method allows direct calculation of pressure transverse.. The Runge-Kutta approximate solution to the differential equation

$$\frac{dy}{dx} = f(x, y) \quad \text{at } x = x_n \quad (20)$$

given that $y = y_o$ when $x = x_o$ is

$$y = y_o + \frac{1}{6}(k_1 + 2(k_2 + k_3) + k_4) \quad (21)$$

where

$$k_1 = Hf(x_o, y_o)$$

$$k_2 = Hf\left(x + \frac{1}{2}H, y_o + \frac{1}{2}k_1\right)$$

$$k_3 = Hf\left(x_o + \frac{1}{2}H, y_o + \frac{1}{2}k_1\right)$$

$$k_4 = Hf(x_o + H, y + k_3)$$

$$H = \frac{x_n - x_o}{n}$$

n = number of applications

The Runge-Kutta algorithm can obtain an accurate solution with a large value of H . The Runge-Kutta Algorithm can solve equation (6) or (12). The test problem used in this work is from the book of Ikoku (1984), "Natural Gas Production Engineering". Ikoku has solved this problem with some of the available methods in the literature.

Example 1

Calculate the sand face pressure (p_{wf}) of a flowing gas well from the following surface measurements.

Flow rate (Q) = 5.153 MMSCF / Day

Tubing internal diameter (d) = 1.9956in

Gas gravity (G_g) = 0.6

Depth = 5790ft (bottom of casing)

Temperature at foot of tubing (T_{wf}) = 160 °F

Surface temperature (T_{sf}) = 83 °F

Tubing head pressure (p_{tf}) = 2122 psia

Absolute roughness of tubing (ϵ) = 0.0006 in

Length of tubing (l) = 5700ft (well is vertical)

Solution

When length (l) is zero, $p = 2122$ psia

That is $(x_o, y_o) = (0, 2122)$

By use of 1 step Runge-Kutta.

$$H = \frac{5700 - 0}{1} = 5700\text{ft.}$$

The Runge-Kutta algorithm is programmed in Fortran 77 and used to solve this problem. The program is also used to study the size of depth(length) increment needed to obtain an accurate solution by use of the Runge-Kutta method. The first output shows result for one-step Runge-Kutta (Depth increment = 5700ft). The program obtains 2544.823 psia as the flowing bottom hole pressure (P_{wf}).

```
TUBING HEAD PRESSURE =      2122.0000000 PSIA
SURFACE TEMPERATURE =      543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH =      620.0000000 DEGREE RANKINE
GAS GRAVITY =      6.0000000E-001
GAS FLOW RATE =      5.1530000 MMSCFD
DEPTH AT SURFACE =      .0000000 FT
TOTAL DEPTH =      5700.0000000 FT
INTERNAL TUBING DIAMETER =      1.9956000 INCHES
ROUGHNESS OF TUBING =      6.0000000E-004 INCHES
INCREMENTAL DEPTH =      5700.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2122.000	.000
2544.823	5700.000

To check the accuracy of the Runge-Kutta algorithm for the depth increment of 5700 ft another run is made with a smaller length increment of 1000 ft. The output gives a p_{wf} of 2544.823 psia. as it is with a depth increment of 5700 ft. This confirms that the Runge-Kutta solution can be accurate for a length increment of 5700 ft.

```
TUBING HEAD PRESSURE =      2122.0000000 PSIA
SURFACE TEMPERATURE =      543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH =      620.0000000 DEGREE RANKINE
GAS GRAVITY =      6.0000000E-001
GAS FLOW RATE =      5.1530000 MMSCFD
DEPTH AT SURFACE =      .0000000 FT
TOTAL DEPTH =      5700.0000000 FT
INTERNAL TUBING DIAMETER =      1.9956000 INCHES
ROUGHNESS OF TUBING =      6.0000000E-004 INCHES
INCREMENTAL DEPTH =      1000.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2122.000	.000
2206.614	1140.000
2291.203	2280.000
2375.767	3420.000
2460.306	4560.000
2544.823	5700.000

In order to determine the maximum length of pipe (depth) for which the computed P_{wf} can be considered as accurate, the depth of the test well is arbitrarily increased to 10,000ft and the program run with one step (length increment = 10,000ft). The program produces the P_{wf} as 2861.060 psia..

```
TUBING HEAD PRESSURE =      2122.0000000 PSIA
SURFACE TEMPERATURE =      543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH =    687.0000000 DEGREE RANKINE
GAS GRAVITY =      6.0000000E-001
GAS FLOW RATE =      5.1530000 MMSCFD
DEPTH AT SURFACE =      .0000000 FT
TOTAL DEPTH =      10000.0000000 FT
INTERNAL TUBING DIAMETER =      1.9956000 INCHES
ROUGHNESS OF TUBING =      6.0000000E-004 INCHES
INCREMENTAL DEPTH =      10000.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2122.000	.000
2861.060	10000.000

Next the total depth of 10000ft is subdivided into ten steps (length increment = 1,000ft). The program gives the P_{wf} as 2861.057 psia for the length increment of 1000ft.

```
TUBING HEAD PRESSURE =      2122.0000000 PSIA
SURFACE TEMPERATURE =      543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH =    687.0000000 DEGREE RANKINE
GAS GRAVITY =      6.0000000E-001
GAS FLOW RATE =      5.1530000 MMSCFD
DEPTH AT SURFACE =      .0000000 FT
TOTAL DEPTH =      10000.0000000 FT
INTERNAL TUBING DIAMETER =      1.9956000 INCHES
ROUGHNESS OF TUBING =      6.0000000E-004 INCHES
INCREMENTAL DEPTH =      1000.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2122.000	.000
2197.863	1000.000
2273.246	2000.000
2348.165	3000.000
2422.638	4000.000
2496.680	5000.000
2570.311	6000.000
2643.547	7000.000
2716.406	8000.000
2788.903	9000.000
2861.057	10000.000

The computed values of P_{wf} for the depth increment of 10,000ft and 1000ft differ only in the third decimal place. This suggests that the depth increment for the Range - Kutta solution to the differential equation generated in this work could be as large as 10,000ft. By neglecting the denominator of equation (6) that accounts for the kinetic effect, the result can be compared with Ikoku's average temperature and gas deviation method that uses an average value of the gas deviation factor (z) and negligible kinetic effects. In the program z is allowed to vary with pressure and temperature. The temperature in the program also varies with depth (length of tubing) as

$$T = GTG \times \text{current length} + T_{sf}, \text{ where, } GTG = \frac{(T_{wf} - T_{sf})}{\text{Total Depth}}$$

The program obtains the P_{wf} as 2544.737 psia when the kinetic effect is ignored. The output is as follows:

```
TUBING HEAD PRESSURE =      2122.0000000 PSIA
SURFACE TEMPERATURE =      543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH =      620.0000000 DEGREE RANKINE
GAS GRAVITY =      6.0000000E-001
GAS FLOW RATE =      5.1530000 MMSCFD
DEPTH AT SURFACE =      .0000000 FT
TOTAL DEPTH =      5700.0000000 FT
INTERNAL TUBING DIAMETER =      1.9956000 INCHES
ROUGHNESS OF TUBING =      6.0000000E-004 INCHES
INCREMENTAL DEPTH =      5700.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2122.000	.000
2544.737	5700.000

Comparing the P_{wf} of 2544.737 psia with the P_{wf} of 2544.823 psia when the kinetic effect is considered, the kinetic contribution to the pressure drop is $2544.823 \text{ psia} - 2544.737 \text{ psia} = 0.086 \text{ psia}$. The kinetic effect during calculation of pressure transverse in uphill dipping pipes is small and can be neglected as pointed out by previous researchers such as Ikoku (1984) and Uoyang and Aziz (1996)

Ikoku obtained 2543 psia by use of the the average temperature and gas deviation method. The average temperature and gas deviation method goes through trial and error calculations in order to obtain an accurate solution. Ikoku also used the Cullendar and Smith method to solve the problem under consideration. The Cullendar and Smith method does not consider the kinetic effect but allows a wide variation of the temperature. The Cullendar and Smith method involves the use of Simpson rule to carry out an integration of a cumbersome function. The solution to the given problem by the Cullendar and Smith method is $p_{wf} = 2544 \text{ psia}$.

If we neglect the denominator of equation (12), then the differential equation for pressure transverse in a flowing gas well becomes

$$\frac{dy}{dl} = A + By \quad (22)$$

where

$$A = \frac{1.621139fW^2zRT}{gd^5M} \quad (23)$$

$$B = \frac{2M \sin \theta}{zRT} = \frac{2 \times 28.79G_g \sin \theta}{RTz} \quad (24)$$

The equation is valid in any consistent set of units. If we assume that the pressure and temperature in the tubing are held constant from the mid section of the pipe to the foot of the tubing, the Runge-Kutta method can be used to obtain the pressure transverse in the tubing as follows.

$$\frac{dy}{dl} = \frac{\frac{46.9643686GgQ_b^2fzRT}{gd^5} + \frac{59.940Gg \sin \theta y}{zRT}}{1 - \frac{46.9643686KzGgQ_b^2}{gRd^4} \left(\frac{P_b}{T_b}\right)^2 \left(\frac{T}{y}\right)} \quad (25)$$

The weight flow rate (W) in equation (12) is related to Q_b (the volumetric rate measurement at a base pressure (P_b) and a base temperature (T_b)) in equation (25) by:

$$W = \gamma_b Q_b \quad (26)$$

Equation (25) is a general differential equation that governs pressure transverse in a gas pipe that conveys gas uphill. When the angle of inclination (θ) is zero, $\sin \theta$ is zero and the differential equation reduces to that of a static gas column. The differential equation (25) is valid in any consistent set of units. The constant $K = 1.0328$ for Nigerian Natural Gas when the unit of pressure is psia.

The classical 4th order Runge Kutta algorithm can be used to provide a formula that serves as a general solution to the differential equation (25). To achieve this, the temperature and gas deviation factors are held constant at some average value, starting from the mid section of the pipe to the inlet end of the pipe. The solution to equation (25) by the Runge Kutta algorithm can be written as:

$$p_1 = \sqrt{p_2^2 + y}. \quad (27)$$

Where

$$\bar{y} = \frac{aa}{6} (1 + x + 0.5x^2 + 0.36x^3) + \frac{P_2^2}{6} (4.96x + 1.48x^2 + 0.72x^3) + \frac{u}{6} (4.96 + 1.96x + 0.72x^2)$$

$$aa = \left(\frac{46.9643686 G_g Q_b^2 f_2 z_2 R T_2}{g d^5} + \frac{57.94 G_g \sin \theta P_2^2}{z_2 T_z R} \right) L$$

$$u = \frac{46.9643686 G_g Q_b^2 f_2 z_{av} T_{av} L}{g d^5}$$

$$x = \frac{57.940 G_g \sin \theta L}{z_{av} T_{av} R}$$

When $Q_b = 0$, equation (27) reduces to the formula for pressure transverse in a static gas column.

In equation (27), the component k_4 in the Runge Kutta method given by $k_4 =$

$H_f(x_0 + H, y + k_3)$ was given some weighting to compensate for the fact that the temperature and gas deviation factor vary between the mid section and the inlet end of the pipe.

Equation (27) can be converted to oil field units. In oil field units in which L is in feet, $R = 1545$, temperature is in $^{\circ}R$, $g = 32.2 \text{ ft/sec}^2$, diameter (d) is in inches, pressure (p) is in pound per square inch (psia), flow rate (Q_b) is in MMSCF / Day, $P_b = 14.7 \text{ psia}$ and $T_b = 520^{\circ} R$, the variables aa , u and x that occur in equation (25) can be written as:

$$u = \frac{25.130920 G_g Q_b^2 f_2 z_{av} T_{av} L}{d^5}$$

$$x = 0.03749 \times \frac{G_g L \sin \theta}{z_{av} T_{av}}$$

The following steps are taken in order to use equation (27) to solve a problem.

1. Evaluate the gas deviation factor at a given pressure and temperature. When equation (27) is used to calculate pressure transverse in a gas well, the given pressure and temperature are the surface temperature and gas exit pressure (tubing head pressure).
2. Evaluate the viscosity of the gas at surface condition. This step is only necessary when calculating pressure transverse in a flowing gas well. It is omitted when static pressure transverse is calculated.
3. Evaluate the Reynolds number and dimensionless friction factor by use of surface properties. This step is also omitted when considering a static gas column.
4. Evaluate the coefficient aa in the formula. This coefficient depends only on surface properties.

5. Evaluate the average pressure (p_{av}) and average temperature (T_{av}).
6. Evaluate the average gas deviation factor. (z_{av})
7. Evaluate the coefficients x and u in the formula. Note that $u = 0$ when $Q_b = 0$.
8. Evaluate \bar{y} in the formula.
9. Evaluate the pressure p_1 . In a flowing gas well, p_1 is the flowing bottom hole pressure. In a static column, it is the static bottom hole pressure.

Equation (27) is tested by using it to solve two problems from the book of Ikoku(1984), "Natural Gas Production Engineering". The first problem involves calculation of the static bottom hole in a gas well. The second involves the calculation of the flowing bottom hole pressure of a gas well.

Example 2

Calculate the static bottom hole pressure of a gas well having a depth of 5790 ft. The gas gravity is 0.6 and the pressure at the well head is 2300 psia. The surface temperature is 83°F and the average flowing temperature is 117°F.

Solution

Following the steps that were listed for the solution to a problem by use of equation (27) we have:

1. Evaluation of z - factor.

The standing equation for P_c and T_c are:

$$P_c \text{ (psia)} = 677.0 + 15.0 G_g - 37.5 G_g^2$$

$$T_c \text{ (°R)} = 168.0 + 325.0 G_g - 12.5 G_g^2$$

Substitution of $G_g = 0.6$ gives, $P_c = 672.5$ psia and $T_c = 358.5^\circ\text{R}$. Then $P_r = 2300/672.5 = 3.42$ and $T_r = 543/358.5 = 1.52$

The Standing and Katz chart gives $z_2 = 0.78$.

Steps 2 and 3 omitted in the static case.

$$4. \quad aa = \left(\frac{25.13092 G_g Q_b^2 f z_2 T_2}{d^5} + \frac{0.037417 G_g p_2^2 \sin \theta}{z_2 T_2} \right) L$$

Here, $G_g = 0.6$, $Q_b = 0.0$, $z_2 = 0.78$, $d = 1.9956$ inches, $p_2 = 2300$ psia,

$T_2 = 543^\circ\text{R}$ and $L = 5790$ ft. Well is vertical, $\theta = 90^\circ$, $\sin \theta = 1$. Substitution of the given values gives:

$$aa = 0.0374917 \times 0.6 \times 2300^2 \times 5790 / (0.78 \times 543) = 1626696$$

5. $p_{av} = \sqrt{2300^2 + 0.5 \times 1626696} = 2470.5$ psia

$$\text{Reduced } p_{av} = 2470.5 / 672.5 = 3.68$$

$$T_{av} = 117^\circ\text{F} = 577^\circ\text{R}$$

Reduced $T_{av} = 577/358.5 = 1.61$

From the standing and Katz chart, $z_{av} = 0.816$

7. In the static case $u = 0$, so we only evaluate x

$$x = \frac{0.0374917 \times 0.6 \times 5790 \sin 90^\circ}{0.816 \times 577} = 0.2766$$

8.
$$\bar{y} = \frac{aa}{6} (1 + x + 0.5x^2 + 0.36x^3) + \frac{P_2^2}{6} (4.96x + 1.48x^2 + 0.72x^3)$$

Substitution of $a = 1626696$, $x = 0.2766$ and $P_2 = 2300$ gives

$$\bar{y} = 358543 + 1322856 = 1681399$$

9.
$$p_1 = \sqrt{p_2^2 + \bar{y}} = (2300^2 + 1681399)^{0.5} = 2640.34 \text{ psia} \approx 2640 \text{ psia}$$

Ikoku used 3 methods to work this problem. His answers of the static bottom hole pressure are:

Average temperature and deviation factor = 2639 psia

Sukkar and Cornell method = 2634 psia

Cullender and Smith method = 2641 psia

The direct calculation formula of this work is faster.

Example 3

Use equation (27) to solve the problem of example 1 that was previously solved by computer programming.

Solution

1. Obtain the gas deviation factor at the surface. From example 2, the pseudocritical properties for a 0.6 gravity gas are, $P_c = 672.5$ psia. and $T_c = 358.5$, then

$$P_r = 2122 / 672.5 = 3.16$$

$$T_r = 543 / 358.5 = 1.52$$

From the Standing and Katz chart, $Z_2 = 0.78$

2. Obtain, the viscosity of the gas at surface condition. By use of Ohirhian and Abu

$$\text{equation, } \mu_g = \frac{0.0059723 p}{z \left(16.393443 - \frac{T}{p} \right)} = \frac{0.0059723 \times 2122}{0.78 \left(16.393443 - \frac{543}{2122} \right)} = 0.9985$$

$$\text{Then } \mu_g = \frac{0.0109388 - 0.008823(0.9985) - 0.0075720(0.9985)^2}{1.0 - 1.3633077(0.9985) - 0.0461989(0.9985)^2} = 0.0133 \text{ cp}$$

3. Evaluation of the Reynolds number and dimensionless friction factor

$$R_N = \frac{20071 Q_b G_g}{\mu_g d} = \frac{20071 \times 5.153 \times 0.6}{0.0133 \times 1.9956} = 2.34 \times 10^6$$

The dimensionless friction factor by Ohirhian formula is

$$f = \left[-2 \log \left(a - 2b \log \left(a + bx_1 \right) \right) \right]^{-2}$$

Where

$$a = \epsilon / 3.7d, \quad b = 2.51 / R_N$$

$$x_1 = -1.14 \log \left(\frac{\epsilon}{d} + 0.30558 \right) + 0.57 \log R_N (0.01772 \log R_N + 1.0693)$$

Substitute of $\epsilon = 0.0006$, $d = 1.9956$, $R_N = 2.34 \times 10^6$ gives $f = 0.01527$

4. Evaluate the coefficient aa in the formula. This coefficient depends only on surface properties.

$$aa = \left(\frac{25.13092 G_g Q_b^2 f z_2 T_2}{d^5} + \frac{0.037417 G_g p_2^2 \sin \theta}{z_2 T_2} \right) L$$

Here, $G_g = 0.6$, $Q_b = 5.153$ MMSCF/Day, $f = 0.01527$, $z_2 = 0.78$, $d = 1.9956$ inches,

$$p_2 = 2122 \text{ psia}, \quad T_2 = 543^\circ \text{R}, \quad z = 5700 \text{ ft}$$

Substitution of the given values gives;

$$aa = (81.817446 + 239.14594) \times 5700 = 1829491$$

5. Evaluate P_{av}

$$p_{av} = \sqrt{p_2^2 + 0.5aa} = \sqrt{2122^2 + 0.5 \times 1829491} = 2327.6 \text{ psia}$$

6. Evaluation of average gas deviation factor.

$$\text{Reduced average pressure} = p_{av} / p_c = 2327.6 / 672.5 = 3.46$$

$$T_{av} = T_2 + \alpha L / 2$$

Where α is the geothermal gradient.

$$\alpha = (T_1 - T_2) / L = (620 - 543) / 5700 = 0.01351$$

T_{av} at the mid section of the pipe is 2850 ft. Then, $T_{av} = 543 + 0.01351 \times 2850 = 581.5^\circ \text{R}$

$$\text{Reduced } T_{av} = 581.5 / 358.5 = 1.62$$

Standing and Katz chart gives $z_{av} = 0.822$

7. Evaluation of the coefficients x and u

$$x = \frac{0.0374917 G_g L}{z_{av} T_{av}} = \frac{0.0374919 \times 0.6 \times 5700}{0.822 \times 581.5} = 0.26824$$

$$u = \frac{25.13092 G_g Q_b^2 f z_{av} T_{av} L}{d^5} = \frac{25.13092 \times 0.6 \times 5.153^2 \times 0.01527 \times 0.822 \times 581.5 \times 5700}{1.9956^5} = 526662$$

8. Evaluate \bar{y}

$$\bar{y} = \frac{aa}{6} (1 + x + 0.5x^2 + 0.36x^3) + \frac{p_2^2}{6} (4.96x + 1.48x^2 + 0.72x^3) + \frac{u}{6} (4.96 + 1.96 + 0.72x^2)$$

Where $u = 526662$, $x = 0.26824$, $p_2 = 2122$ psia and $aa = 1829491$. Then,

$$\bar{y} = 399794 + 1088840 + 485752 = 1974386 \text{ psia}^2$$

9. Evaluate p_1 (the flowing bottom hole pressure)

$$p_1 = \sqrt{p_2^2 + \bar{y}}$$

$$= \sqrt{2122^2 + 1974386} = 2545.05 \text{ psia}$$

$$\approx 2545 \text{ psia}$$

The computer program obtains, the flowing bottom hole pressure as 2544.823 psia. For comparison with other methods of solution, the flowing bottom hole pressure by:

Average Temperature and Deviation Factor, $P_1 = 2543$ psia

Cullender and Smith, $P_1 = 2544$

The direct calculating formula of this work is faster. The Cullendar and Smith method is even more cumbersome than that of Ikoku. It involves the use of special tables and charts (Ikoku, 1984) page 338 - 344.

The differential equation for static gas behaviour and its downhill flow in pipes

The problem of calculating pressure transverse during downhill gas flow in pipes is encountered in the transportation of gas to the market and in gas injection operations. In the literature, models for pressure prediction during downhill gas flow are rare and in many instances the same equations for uphill flow are used for downhill flow.

In this section, we present the use of the Runge-Kutta solution to the downhill gas flow differential equation.

During downhill gas flow in pipes, the negative sign in the numerator of differential equation (12) is used. The differential equation also breaks down to a simple differential equation for pressure transverse in static columns when the flow rate is zero. The equation to be solved is:

$$\frac{dy}{dl} = \frac{(A - By)}{(1 - \frac{G}{y})} \tag{28}$$

Where $y = p^2$,

$$A = \frac{1.621139 f W^2 zRT}{gd^5 M}, \quad B = \frac{2M \sin \theta}{zRT}, \quad G = \frac{KW^2 zRT}{gMd^4}$$

Also, the molecular weight (M) of a gas, can be expressed as $M = 28.97Gg$.

Then, the differential equation (28) can be written as:

$$\frac{dP^2}{d\ell} = \frac{\left[\frac{0.0559592 f z R T W^2}{g d^5 G_g} - \frac{59.940 G_g \sin \theta P^2}{z R T} \right]}{\left[1 - \frac{0.0559592 z R T W^2 K}{g d^5 G_g P^2} \right]} \quad (29)$$

The differential equation (29) is valid in any consistent set of units. The relationship between weight flow rate (W) and the volumetric flow rate measured at a base condition of pressure and temperature (Q_b) is;

$$W = \gamma_b Q_b \quad (30)$$

The specific weight at base condition is:

$$\gamma_b = \frac{p_b M}{z_b T_b R} = \frac{28.97 G_g p_b}{z_b T_b R} \quad (31)$$

Substitution of equations (30) and (31) into differential equation (29) gives:

$$\frac{dp^2}{d\ell} = \frac{\left[\frac{46.9583259 f z T G_g P_b^2 Q_b^2}{g d^5 z_b^2 T_b^2 R} - \frac{59.940 G_g \sin \theta P^2}{z R T} \right]}{\left[1 - \frac{46.95832593 G_g Q_b^2 K}{g R d^4} \left(\frac{P_b}{T_b} \right)^2 \left(\frac{T}{P^2} \right) \right]} \quad (32)$$

The differential equation (32) is also valid in any consistent set of units.

Solution to the differential equation for downhill flow

In order to find a solution to the differential equation for downhill flow (as presented in equation (29) and (32)) we need equations or charts that can provide values of the variables z and f . The widely accepted chart for the values of the gas deviation factor (z) is that of Standing and Katz (1942). The chart has been curve fitted by some researchers. The version used in this section is that of Ohirhian (1993). The Ohirhian set of equations are able to read the chart within $\pm 0.777\%$ error. The Standing and Katz charts require reduced pressure (P_r) and reduced temperature (T_r). The P_r is defined as $P_r = P/P_c$ and the T_r is defined as $T_r = T/T_c$; where P_c and T_c are pseudo critical pressure and pseudo critical temperature, respectively.

Standing (1977) has presented equations for P_c and T_c as functions of gas gravity (G_g). The equations are:

$$P_c = 677 + 15.0 G_g - 37.5 G_g^2 \quad (33)$$

$$T_c = 168 + 325 G_g - 12.5 G_g^2 \quad (34)$$

The differential equation for the downhill gas flow can also be solved by the classical fourth order Runge-Kutta method.

The downhill flow differential equation was tested by reversing the direction of flow in the problem solved in example 3.

Example 4

Calculate the sand face pressure (p_{wf}) of an injection gas well from the following surface measurements.

Flow rate (Q) = 5.153 MMSCF / Day
 Tubing internal diameter (d) = 1.9956 in
 Gas gravity (G_g) = 0.6
 Depth = 5790ft (bottom of casing)
 Temperature at foot of tubing (T_{wf}) = 160°F
 Surface temperature (T_{sf}) = 83°F
 Tubing head pressure (P_{sf}) = 2545 psia
 Absolute roughness of tubing (ϵ) = 0.0006in
 Length of tubing (L) = 5700ft (well is vertical)

Solution

Here, $(x_0, y_0) = (0, 2545)$

By use of I step Runge-Kutta.

$$H = \frac{(5700 - 0)}{1} = 5700$$

The Runge-Kutta algorithm is programmed in Fortran 77 to solve this problem. The output is as follows.

```
TUBING HEAD PRESSURE = 2545.0000000 PSIA
SURFACE TEMPERATURE = 543.0000000 DEGREE RANKINE
TEMPERATURE AT TOTAL DEPTH = 620.0000000 DEGREE RANKINE
GAS GRAVITY = 6.0000000E-001
GAS FLOW RATE = 5.1530000 MMSCFD
DEPTH AT SURFACE = .0000000 FT
TOTAL DEPTH = 5700.0000000 FT
INTERNAL TUBING DIAMETER = 1.9956000 INCHES
ROUGHNESS OF TUBING = 6.0000000E-004 INCHES
INCREMENTAL DEPTH = 5700.0000000 FT
```

PRESSURE PSIA	DEPTH FT
2545.000	.000
2327.930	5700.000

The other outputs from the program (not shown here) indicates that the contribution of kinetic effect to pressure transverse during down hill flow is also negligible. The program also shows that an incremental length as large as 5700 ft can yield accurate result in pressure transverse calculations.

Neglecting the kinetic effect, the Runge-Kutta algorithm can be used to provide a solution to the differential equation (32) as follows

$$p_1 = \sqrt{p_2^2 - |\bar{y}|} \quad (35)$$

Here

$$\bar{y} = \frac{aa}{6} (1 - x + 0.5x^2 + 0.3x^3) + \frac{P_1^2}{6} (-5.2x + 2.2x^2 - 0.6x^3) + \frac{u}{6} (5.2 - 2.2x + 0.6x^2)$$

$$aa = \left(\frac{46.958326 f_1 z_1 T_1 G_g P_b^2 Q_b^2}{gd^5 z_b^2 T_b^2 R} - \frac{57.940 G_g \sin \theta p_1^2}{z_1 T_1 R} \right) L$$

$$u = \frac{46.958326 f_1 z_{av} T_{av} G_g P_b^2 Q_b^2 L}{gd^5 z_b^2 T_b^2 R}, \quad x = \frac{57.940 G_g \sin \theta L}{z_{av} T_{av} R}$$

f_1 = Moody friction factor evaluated at inlet end pipe

T_1 = Temperature at inlet end of pipe

T_{av} = Temperature at mid section of pipe = $0.5(T_1 + T_2)$

p_1 = Pressure at inlet end of pipe

z_1 = Gas deviation factor evaluated with p_1 and T_1

z_{av} = Gas deviation factor calculated with temperature at mid section (T_{av}) and pressure

at the mid section of pipe (p_{av}) given by $p_{av} = \sqrt{p_1^2 - 0.5|aa|}$

p_2 = Pressure at exit end of pipe, psia

p_1 = Pressure at inlet end of pipe

Note that $p_1 > p_2$ and flows occurs from point (1) to point (2)

Equation (35) is valid in any consistent set of units.

Equation (35) can be converted to oil field units. In oil field units in which L is in feet, R = 1545, temperature(T) is in °R, $g = 32.2$ ft/sec², diameter (d) is in inches, pressure (p) is in pound per square inch (psia), flow rate (Q_b) is in MMSCF / Day and $P_b = 14.7$ psia, $T_b = 520^\circ$ R. The variables aa, u and x that occur in equation (35) can be written as:

$$aa = \left(\frac{25.1472069 G_g f_1 z_1 T_1 Q_b^2}{d^5} - \frac{0.0375016 G_g \sin \theta p_1^2}{z_1 T_1} \right) L$$

$$u = \frac{25.1472069 G_g f_1 z_{av} T_{av} Q_b^2 L}{d^5}, \quad x = \frac{0.0375016 G_g \sin \theta L}{z_{av} T_{av}}$$

Example 5

Use equation (35) to solve the problem of example 4

Solution

Step 1: obtain the gas deviation factor at the inlet end

$$T_1 = 83^\circ\text{F} = 543^\circ\text{R}$$

$$P_1 = 2545 \text{ psia}$$

$$G_g = 0.6$$

By use of equation (33) and (34)

$$P_c \text{ (psia)} = 677 + 15 \times 0.6 - 37.5 \times 0.6^2 = 672.5 \text{ psia}$$

$$T_c \text{ (}^\circ\text{R)} = 168 + 325 \times 0.6 - 12.5 \times 0.6^2 = 358.5 \text{ }^\circ\text{R}$$

$$\text{Then, } P_{1r} = 2545/672.5 = 3.784, T_{1r} = 543/358.5 = 1.515$$

The required Ohirhian equation is

$$z = \left(z_1 + \left(1.39022 + \text{Pr} (0.06202 - 0.02113 \times \text{Pr}) \right) \times \log \text{Tr} \right) F_c$$

Where

$$z_1 = 0.60163 + \text{Pr} (-0.06533 + 0.0133\text{Pr})$$

$$F_c = 20.208372 + \text{Tr} (-44.0548 + \text{Tr} (37.55915 + \text{Tr} (-14.105177 + 1.9688\text{Tr})))$$

Substitution of values of $\text{Pr} = 3.784$ and $\text{Tr} = 1.515$ gives $z = 0.780588$

Step 2

Evaluate the viscosity of the gas at inlet condition. By use of Ohirhian and Abu formula (equation 17)

$$xx = \frac{0.0059723 \times 2545}{0.780588 (16.393443 - 543/2545)} = 1.203446$$

$$\mu_g = \frac{0.0109388 - 0.008823 (1.203446) - 0.0075720 (1.203446)^2}{1.0 - 1.3633077 (1.203446) - 0.0461989 (1.203446)^2} = 0.015045 \text{ cp}$$

Step 3

Evaluation of Reynolds number (R_N) and dimensionless friction factor (f). From eqn. (26)

$$R_N = \frac{20071 \times 5.153 \times 0.6}{0.015045 \times 1.9956} = 2066877$$

The dimensionless friction factor can be explicitly evaluated by use of Ohirhian formula (equation 19)

$$\epsilon/d = 0.0006/1.9956 = 3.066146\text{E} - 4$$

$$a = 3.066146\text{E} - 4/3.7 = 8.125985\text{E} - 5$$

$$b = 2.51/2066877 = 1.21393\text{E} - 6$$

$$x_1 = -1.14 \log (3.066146\text{E} - 4 + 0.30558) + 0.57 \times \log 2066877 (0.01772 \log 2066877 + 1.0693) = 4.838498$$

Substitution of values of a , b and x_1 into $f = \left[-2 \log (a - 2b \log (a + bh)) \right]^{-2}$ gives

$$f = 0.01765$$

Step 4

Evaluate the coefficient aa in the formula. This coefficient depends only on surface (inlet) properties. Note that the pipe is vertical $\theta = 90^\circ$ and $\sin 90^\circ = 1$

$$aa = \left(25.147207 \times 0.6 \times 0.017650 \times 0.780588 \times 543 \times 5.153^2 \times 5700 \right) / 1.9956^5 \\ - \left(0.037502 \times 0.6 \times 1 \times 2545 \times 5700 \right) / (0.780588 \times 543) \\ = 539803 - 1959902 = -1420099$$

Step 5

Evaluate the average pressure (p_{av}) at the mid section of the pipe given by

$$p_{av} = \sqrt{p_1^2 - 0.5|aa|} = \sqrt{2545^2 - 0.5 \times 1420099} = 2401.5$$

Step 6:

Evaluate the average gas deviation factor (z_{av}). Reduced average pressure (p_{avr}) = $2401.5/672.5 = 3.571$. $T_{av} = T_1 + \alpha L/2$ where α = geothermal gradient given by :

$$\alpha = (T_2 - T_1) / L = (620 - 543) / 5700 = 0.013509$$

T_{av} at mid section of pipe (2850 ft) then, is: $T_{av} = 543 + 0.013509 \times 2850 = 581.5^\circ R$

Reduced $T_{av} = 581.5/358.5 = 1.622$

Substitution into the Ohirhian equation used in step 1, gives $z = 0.821102$

Step 7:

Evaluate the coefficients x and u

$$x = \frac{0.0375016 \times 0.6 \times 1 \times 5700}{0.821102 \times 581.5} = 0.268614$$

$$u = \left(25.147207 \times 0.6 \times 0.017650 \times 0.821102 \times 581.5 \times 5.153^2 \times 5700 \right) / 1.9956^5 = 608079$$

Step 8: Evaluate \bar{y}

$$\bar{y} = \frac{u}{6} (5.2 - 2.2x + 0.6x^2) + \frac{p_1^2}{6} (-5.2x + 2.2x^2 - 0.6x^3) + \frac{aa}{6} (1 - x + 0.5x^2 - 0.3x^3)$$

Substitution of $u = 608079$, $p_1 = 2545$ psia, $aa = -1420099$ and $x = 0.268614$ gives

$$\bar{y} = 471499 - 1349039 - 180269 = -1057809$$

Step 9: Evaluate p_2 , the pressure at the exit end of the pipe

$$P_2 = \sqrt{(2545^2 - 1057809)} = 2327.92 \text{ psia} \approx 2328 \text{ psia}$$

Pressure drop across 5700 ft of tubing is $2545 \text{ psia} - 2328 \text{ psia} = 217 \text{ psia}$

This pressure drop may be compared with the pressure drop across the 5700 ft of tubing when gas flows uphill against the force of gravity. From example 3, tubing pressure at the surface = 2122 psia when the bottom hole pressure (inlet pressure) = 2545 psia. Then pressure drop = $2545 \text{ psia} - 2122 \text{ psia} = 423 \text{ psia}$. The pressure drop during down hill flow is less than that during up hill flow.

The general solution (valid in any system of units) to the differential equation for downhill flow was tested with slight modification of a problem from the book of Giles et al (2009). In the original problem the pipe was horizontal. In the modification used in this work, the pipe

was made to incline at 10 degrees from the horizontal in the downhill direction. Other data remained as they were in the book of Giles et al.. The data are as follows:

Example 6

Given the following data,

Length of pipe (L) = 1800ft

$Z_2 = Z_1 = Z_{av} = 1$ (air is flowing fluid)

$p_1 = 49.5 \text{ psia} = 49.5 \times 144 \text{ psf} = 7128 \text{ psf}$

$W = 0.75 \text{ lb/sec}$

$Q_b = 9.81937 \text{ ft}^3/\text{sec}$

$P_b = 14.7 \text{ psia} = 2116.8 \text{ psf}$

$T_b = 60 \text{ }^\circ\text{F} = 520 \text{ }^\circ\text{R}$

$T_1 = T_{av} = 90 \text{ }^\circ\text{F} = 550 \text{ }^\circ\text{R}$

$G_g = 1.0$ (air)

$R = 1544$

$\mu = 390 \times 10^{-9} \text{ lb sec/ft}^2$

$d = 4 \text{ inch} = 0.333333 \text{ ft}$

Absolute Roughness (ϵ) = 0.0003 ft

calculate the exit pressure (p_2) at 1800 ft of pipe.

Solution

Step 1: Obtain the gas elevation factor at inlet end, $z_1 = 1.0$, air in flowing fluid

Step 2: Obtain the viscosity of the gas at inlet condition. Viscosity of gas is $390 \times 10^{-9} \text{ lb sec / ft}^2$ (given)

Step 3: Evaluate the Reynolds number and friction factor.

$$R_N = \frac{36.88575 G_g P_b Q_b}{g R d \mu z_b T_b}$$

Here, $G_g = 1.0$ (air), $P_b = 2116.8 \text{ psf}$, $Q_b = 9.81937 \text{ ft}^3 / \text{sec}$, $g = 32.2 \text{ ft / sec}^2$, $d = 0.33333 \text{ ft}$,

$R = 1544$, $\mu = 390 \times 10^{-9}$, $z_b = 1.0$ (air), $T_b = 520 \text{ }^\circ\text{R}$

Then

$$R_N = \frac{36.88575 \times 1 \times 2116.8 \times 9.81937 \times 10^9}{32.2 \times 1544 \times 0.3333 \times 390 \times 1 \times 520} = 2281249$$

$$\frac{\epsilon}{d} = \frac{0.0003}{0.33333} = 0.0009$$

From Moody chart, $f_1 = 0.0205$

Step 4: Evaluate the coefficient aa in the formula

$$aa = \left(\frac{46.958326 f_1 z_1 T_1 G_g P_b^2 Q_b^2}{g d^5 z_b^2 T_b^2 R} - \frac{57.940 G_g \sin \theta P_1^2}{z_1 T_1 R} \right) L$$

$$\frac{46.958326 \times 0.0205 \times 1 \times 550 \times 1 \times 2116.8^2 \times 9.81937^2}{32.2 \times 0.33333^5 \times 520^2 \times 1544} = 4134.70$$

$$\frac{57.94 \times 1 \times 0.173648 \times 7128^2}{1 \times 550 \times 1544} = \frac{511191540.9}{849200} = 601.97$$

Then $aa = (4134.70 - 601.97) \times 1800 = 6358914$

Step 5

Evaluate the average pressure (p_{av}) at the mid section of the pipe

$$p_{av} = \sqrt{p_1^2 - 0.5 \times 6358914} = 6901.4 \text{ psf}$$

Step 6: Evaluate average gas derivation factor (Z_{av}) for air, $z_{av} = 1.0$

Step 7: Evaluate the coefficients x and u

$$x = \frac{57.94 G_g \sin \theta L}{z_{av} T_{av} R} = \frac{57.94 \times 1 \times 0.173648 \times 1800}{1 \times 550 \times 1544} = 0.021326$$

$$u = \frac{46.958326 f_1 z_{av} T_{av} G_g P_b^2 Q_b^2 L}{g d^5 z_b^2 T_b^2 R} = \frac{46.958326 \times 0.0205 \times 1 \times 550 \times 1 \times 2116.8^2 \times 9.81937^2 \times 1800}{32.2 \times 0.33333^5 \times 1 \times 520^2 \times 1544} = 7442642.4$$

Step 8: Evaluate \bar{y}

$$\bar{y} = \frac{u}{6} (5.2 - 2.2x + 0.6x^2) + \frac{p_1^2}{6} (-5.2x + 2.2x^2 - 0.6x^3) + \frac{aa}{6} (1 - x + 0.5x^2 - 0.3x^3)$$

Where $x = 0.021326$, $(5.2 - 2.2x + 0.6x^2) = 5.153356$, $(-5.2x + 2.2x^2 - 0.6x^3) = -0.10990$
 $(1 - x + 0.5x^2 - 0.3x^3) = 0.9789$.

$$\begin{aligned} \text{Then, } \bar{y} &= \frac{7442642.4}{6} \times 5.153356 + \frac{7128^2}{8} (-0.1099) + \frac{6358914}{6} (0.9789) \\ &= 6392431 - 930644 + 1037457 = 6499244 \end{aligned}$$

Step 9: Evaluate p_2 , the pressure at the exit end of the pipe

$$p_2 = \sqrt{7128^2 - 6499244} = 6656.5 \text{ psf} = \frac{6656.5 \text{ psia}}{144} = 46.2 \text{ psia}$$

Pressure drop = 49.5 psia - 46.2 psia = 3.3 psia

When the pipe is horizontal, p_2 (from Fluid Mechanics and Hydraulics) is 45.7 psia. Then, pressure drop = 49.5 psia - 45.7 psia = 3.8 psia

Direct calculation of the gas volumetric rate

The rate of gas flow through a pipe can be calculated if the pipe properties, the gas properties, the inlet and outlet pressures are known. The gas volumetric rate is obtained by solving an equation of pressure transverse simultaneously with the Reynolds number and the Colebrook friction factor equation.

Direct calculation of the gas rate in uphill pipes

Ohirhian(2002) combined the Weymouth equation with the Reynolds number and the Colebrook friction factor equation to arrive at an equation for the direct calculation of the gas volumetric rate during uphill gas flow. In this section, the formula type solution to the differential equation for horizontal and uphill gas flow is combined with the Reynolds number and the Colebrook equation to arrive at another equation for calculating the gas volumetric rate during uphill gas flow.

Combination of the pressure transverse formula for uphill gas flow (equation (27) in oil field units, with the Reynolds number, equation (16) and equation (18) which is the Colebrook friction factor equation, leads to:

$$\frac{1}{\sqrt{f}} = -2 \log\left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha}\right) \dots (36)$$

$$R_N = -2 \alpha \log\left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha}\right) \dots (37)$$

$$Q_b = \frac{-\mu_2 d R_N}{20071 G_g} = \frac{-2 \mu_2 d \alpha}{20071 G_g} \log\left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha}\right) \dots (38)$$

$$\alpha = \frac{20071 G_g \left[p_1^2 - p_2^2 \left(1 + \frac{x_b}{6}\right) - \frac{1}{6}(S L x_a) \right]^{0.5}}{\mu_2 d \sqrt{B} [z_2 T_2 x_a + z_{av} T_{av} x_c]^{0.5}}$$

Where,

$$x = \frac{0.0375016 G_g \sin \theta L}{z_{av} T_{av}}$$

$$B = \frac{4.191201 G_g L}{d^5}$$

$$S = \frac{0.03075016 G_g \sin \theta p_2^2}{z_2 T_2}$$

z_{av} is computed with $T_{av} = 0.5(T_1 + T_2)$ and $p_{av}^2 = 0.5(p_1^2 + p_2^2)$.

μ_2 is viscosity of gas at p_2 and T_2 . The subscript 2 refers to surface condition.

$$x_a = 1 + x + 0.5x^2 + 0.36x^3$$

$$x_b = 4.96x + 1.48x^2 + 0.72x^3$$

$$x_c = 4.96 + 1.96x + 0.72x^2$$

The above equations are in oil field units in which d is expressed in inches, L in feet, μ in centipoises, T in degrees rankine and pressure in pounds per square inches. In this system of units, $p_b = 14.7$ psia, $T_b = 520$ ° R, $z_b = 1.0$. The subscript 2 refers to surface condition in the gas well.

Example 7

A gas well has the following data:

$L = 5700$ ft, $G_g = 0.6$, $\theta = 90$ °, $Z_2 = 0.78$, $Z_{av} = 0.821$, $f = 0.0176$, $T_2 = 543$ ° R,

$T_{av} = 581.5$ ° R, $d = 1.9956$ in, absolute roughness of pipe = 0.0006 in, $p_1 = 2545$ psia, $p_2 = 2122$ psia, μ_2 , viscosity of gas at p_2 and $T_2 = 0.0133$ cp. Calculate the flow rate of the well (Q_b) in MM SCF / Day,

Solution

Substituting given values,

$$x = 0.0375016 \times \frac{0.6 \times 1 \times 5700}{0.822 \times 581.5} = 0.268250$$

$$B = 4.191201 \times \frac{0.6 \times 5700}{1.9956^5} = 452.6012689$$

$$S = 0.0375016 \times \frac{0.6 \times 1 \times 2122^2}{0.78 \times 543} = 238.680281$$

$$x_a = 1 + x + 0.5x^2 + 0.36x^3 = 1 + 0.268250 + 0.5 \times 0.268250^2 + 0.36 \times 0.268250^3 = 1.311178$$

$$x_b = 4.96x + 1.48x^2 + 0.72x^3 = 4.96 \times 0.268250 + 1.48 \times 0.268250^2 + 0.72 \times 0.268250^3 = 1.45096$$

$$x_c = 4.96 + 1.96x + 0.72x^2 = 4.96 + 1.96 \times 0.268250 + 0.72 \times 0.268250^2 = 5.53758$$

$$\alpha = \frac{20071 \times 0.6 \left[2545^2 - 2122^2 \left(1 + \frac{1.45096}{6} \right) - \frac{1}{6} (238.680281 \times 5700 \times 1.311178) \right]^{0.5}}{0.0133 \times 1.9956 \sqrt{452.6012689} [1.45096 \times 0.78 \times 543 + 0.822 \times 581.5 \times 5.53758]^{0.5}} = 288996.2$$

From example 3, actual Reynolds number is 2.34E06 and $f = 0.01527$. Then,

$$\alpha = R_N \sqrt{f} = 234000 \times \sqrt{0.01527} = 289158.1$$

$$Q_b = \frac{-2 \mu_2 d \alpha}{20071 G_g} \log \left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha} \right) = \frac{-2 \times 0.0133 \times 1.9956 \times 288996.2}{20071 \times 0.6} \times \log \left(\frac{0.0006}{3.7 \times 1.9956} + \frac{2.51}{288996.2} \right) = 5.154 \text{ MMSCF / Day}$$

Direct calculation of the gas volumetric rate in downhill flow

Combination of equation (35) in oil field units, with the Reynolds number, equation (16) and equation (17) which is the Colebrook friction factor equation, leads to:

$$\frac{1}{\sqrt{f}} = -2 \log \left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha_1} \right) \dots \dots (39)$$

$$R_N = -2 \alpha_1 \log \left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha_1} \right) \dots \dots (40)$$

$$Q_b = \frac{-\mu_{av} d R_N}{20071 G_g} = \frac{-2 \mu_{av} d \alpha_1}{20071 G_g} \log \left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha_1} \right) \dots \dots (40)$$

$$\alpha_1 = \frac{20071 G_g \left[J + \frac{1}{6} (S L x_d) \right]^{0.5}}{\mu_1 d \sqrt{B} [z_1 T_1 x_d + z_{av} T_{av} x_f]^{0.5}} \dots \dots (41)$$

$$J = p_2^2 - p_1^2 \left(1 + \frac{x_e}{6} \right), \text{ if } B \geq S \dots \dots (42a)$$

$$J = p_1^2 \left(1 - \frac{x_e}{6} \right) - p_2^2, \text{ if } B < S \dots \dots (42b)$$

$$x_d = 1 - x + 0.5x^2 + 0.3x^3$$

$$x_e = -5.2x + 2.2x^2 - 0.6x^3$$

$$x_f = 5.2 - 2.2x + 0.6x^2$$

$$B = \frac{4.191201 G_g L}{d^5}$$

$$S = \frac{0.03075016 G_g \sin \theta p_1^2}{z_1 T_1}$$

$$x = \frac{0.0375016 G_g \sin \theta L}{z_{av} T_{av}}$$

z_{av} and μ_{av} are evaluated with $T_{av} = 0.5(T_1 + T_2)$ and $p_{av} = (2p_1 p_2) / (p_1 + p_2)$

The subscript 1 refers to surface condition and 2 to exit condition in the gas injection well. The above equations are in oil field units in which d is expressed in inches, L in feet, μ in centipoises, T in degrees rankine and pressure in pounds per square inches. In this system of units, $p_b = 14.7$ psia, $T_b = 520$ °R, $z_b = 1.0$. The subscript 2 refers to surface condition in the gas well.

Example 8

A gas injection well has the following data:

$L = 5700$ ft, $G_g = 0.6$, $\theta = 90$ °, $\sin 90^\circ = 1$, $z_1 = 0.78059$, $Z_{av} = 0.821$, $T_1 = 543$ °R,

$T_{av} = 543$ °R, $d = 1.9956$ in, $p_1 = 2545$ psia, $p_2 = 2327.92$ psia, absolute roughness of tubing (ϵ) = 0.0006 in. Calculate the gas injection rate in MMSCF / Day. Take the viscosity of the at surface condition (μ_1) as 0.015045 cp and the average viscosity of the gas (μ_{av}) as 0.0142 cp.

Solution

$$x = 0.0375016 \times \frac{0.6 \times 1 \times 5700}{0.821 \times 581.5} = 0.26865$$

$$B = 4.191201 \times \frac{0.6 \times 5700}{1.9956^5} = 452.89458$$

$$S = 0.0375016 \times \frac{0.6 \times 1 \times 2545^2}{0.78059 \times 543} = 343.83795$$

$$x_d = 1 - x + 0.5x^2 + 0.3x^3 = 1 - 0.26865 + 0.5 \times 0.26865^2 + 0.36 \times 0.26865^3 = 0.76162$$

$$x_e = -5.2x + 2.2x^2 - 0.6x^3$$

$$= -5.2 \times 0.26865 + 2.2 \times 0.26865^2 - 0.6 \times 0.26865^3$$

$$= -1.24982$$

$$x_f = 5.2 - 2.2x + 0.6x^2 =$$

$$5.2 - 2.2 \times 0.26865 + 0.60 \times 26865^2 = 4.65228$$

Since $B > S$, $J = p_2^2 - p_1^2 \left(1 + \frac{x_e}{6}\right)$ is used

$$J = 2327.92^2 - 2545^2 \left(1 - \frac{1.24982}{6}\right) = 291372.42$$

$$\frac{1}{6}(S L x_d) = \frac{1}{6}(343.83795 \times 5700 \times 0.76162) = 248780.17$$

$$\begin{aligned} & \left[z_1 T_1 x_d + z_{av} T_{av} x_f \right]^{0.5} = \\ & (0.78 \times 543 \times 0.76162 + 0.821 \times 581.5 \times 4.65228)^{0.5} \\ & = 50.43440 \end{aligned}$$

$$\begin{aligned} \alpha &= \frac{20071 G_g \left[J + \frac{1}{6}(S L x_d) \right]^{0.5}}{\mu_1 d \sqrt{B} \left[z_1 T_1 x_d + z_{av} T_{av} x_f \right]^{0.5}} \\ &= \frac{20071 \times 0.6 \left[291372.42 + 248780.17 \right]^{0.5}}{0.015045 \times 1.9956 \times \sqrt{452.89458} \times 50.43440} = 274641.7 \end{aligned}$$

From example 5, actual Reynolds number is 2066877 and $f = 0.01765$. Then,

$$\alpha = R_N \sqrt{f} = 2066877 \times \sqrt{0.01765} = 274591.4$$

$$\begin{aligned} Q_b &= \frac{-2 \mu_{av} d \alpha}{20071 G_g} \log \left(\frac{\epsilon}{3.7 d} + \frac{2.51}{\alpha} \right) = \frac{-2 \times 0.0142 \times 1.9956 \times 274641.7}{20071 \times 0.6} \times \log \left(\frac{0.0006}{3.7 \times 1.9956} + \frac{2.51}{274641.7} \right) \\ &= 5.227 \text{ MMSCF / Day} \end{aligned}$$

By use of an average viscosity of 0.0140 cp, the calculated $Q_b = 5.153$ MMSCF / Day. Taking 0.0140 cp as the accurate value of the average gas viscosity, the absolute error in estimated average viscosity is $(0.0002 / 0.014 = 1.43 \%)$. The equation for the gas volumetric rate is very sensitive to values of the average gas viscosity. Accurate values of the average gas viscosity should be used in the direct calculation of the gas volumetric rate.

Conclusions

1. A general differential equation that governs static behavior of any fluid and its flow in horizontal, uphill and downhill pipes has been developed.
2. classical fourth order Runge-Kutta numerical method is programmed in Fortran 77, to test the equation and results are accurate. The program shows that a length increment as large as 10,000 ft can be used in the Runge-Kutta method of solution to differential equation during uphill gas flow and up to 5700ft for downhill gas flow
3. The Runge-Kutta method was used to generate a formulas suitable to the direct calculation of pressure transverse in static gas pipes and pipes that transport gas uphill or downhill. The formulas yield very close results to other tedious methods available in the literature.

4. The direct pressure transverse formulas developed are suitable for wells and pipelines with large temperature gradients.
5. Contribution of kinetic effect to pressure transverse in pipes that transport gas is small and can be neglected..
6. The pressure transverse formulas developed in this work are combined with the Reynolds number and Colebrook friction factor equation to provide accurate formulas for the direct calculation of the gas volumetric rate. The direct calculating formulas are applicable to gas flow in uphill and downhill pipes.

Nomenclature

- p = Pressure
 γ = Specific weight of flowing fluid
 v = Average fluid velocity
 g = Acceleration due to gravity in a consistent set of units.
 $d\ell$ = Change in length of pipe
 θ = Angel of pipe inclination with the horizontal, degrees
 dh_1 = Incremental pressure head loss
 f = Dimensionless friction factor
 L = Length of pipe
 d = Internal diameter of pipe
 W = Weight flow rate of fluid
 C_f = Compressibility of a fluid
 C_g = Compressibility of a gas
 K = Constant for expressing the compressibility of a gas
 M = Molecular weight of gas
 T = Temperature
 R_N = Reynolds number
 ρ = Mass density of a fluid
 μ = Absolute viscosity of a fluid
 z = Gas deviation factor
 R = Universal gas constant in a consistent set of units.
 Q_b = Gas volumetric flow rate referred to P_b and T_b ,
 γ_b = specific weight of the gas at p_b and T_b
 p_b = Base pressure, absolute unit
 T_b = Base temperature, absolute unit
 z_b = Gas deviation at p_b and T_b usually taken as 1
 G_g = Specific gravity of gas (air = 1) at standard condition
 μ_g = Absolute viscosity of a gas
 ϵ = Absolute roughness of tubing
 GTG = Geothermal gradient
 f_2 = Moody friction factor evaluated at outlet end of pipe.

Z_2 = Gas deviation factor calculated with exit pressure and temperature of gas

Z_1 = Gas deviation factor calculated with inlet pressure and temperature of gas

p_2 = Pressure at exit end of pipe.

p_1 = Pressure at inlet end of pipe $p_1 > p_2$

T_2 = Temperature at exit end of pipe

T_1 = Temperature at inlet end of pipe

$T_{av} = 0.5(T_1 + T_2)$

Z_{av} = Gas deviation factor evaluated with T_{av} and average pressure (p_{av}) given

by $p_{av} = \sqrt{p_2^2 + 0.5aa}$ in uphill flow, and $p_{av} = \sqrt{p_1^2 - 0.5|aa|}$
in downhill flow

SI Metric Conversion Factors

$$(^{\circ}\text{F} - 32) / 18 = ^{\circ}\text{C}$$

$$\text{ft} \times 3.048000 \text{ *E-01} = \text{m}$$

$$\text{m} \times 2.540 \text{ * E} + 00 = \text{cm}$$

$$\text{lbf} \times 4.448222 \text{ E} + 00 = \text{N}$$

$$\text{lbm} \times 4.535924 \text{ E} - 01 = \text{kg}$$

$$\text{psi} \times 6.894757 \text{ E} + 03 = \text{Pa}$$

$$\text{lb sec} / \text{ft}^2 \times 4.788026 \text{ E} + 01 = \text{Pa.s}$$

$$\text{cp} \times 1.0 \text{ E} - 3 = \text{Pas}$$

$$\text{foot}^3 / \text{second} (\text{ft}^3 / \text{sec}) \times 2.831685 \text{ E} - 02 = \text{metre}^3 / \text{sec} (\text{m}^3 / \text{s})$$

$$\text{foot}^3 / \text{second} \times 8.64 \text{ *E} - 02 = \text{MMSCF} / \text{Day}$$

$$\text{MMSCF} / \text{Day} \times 1.157407 \text{ E} + 01 = \text{foot}^3 / \text{second} (\text{ft}^3 / \text{sec})$$

$$\text{MMSCF} / \text{Day} \times 3.2774132 \text{ E} + 01 = \text{metre}^3 / \text{sec} (\text{m}^3 / \text{s})$$

$$\text{MMSCF} / \text{Day} = 4.166667 \text{ E} + 04 \text{ ft}^3 / \text{hr}$$

$$\text{ft}^3 / \text{hr} = 7.865792 \text{ E} - 06 \text{ m}^3 / \text{s}$$

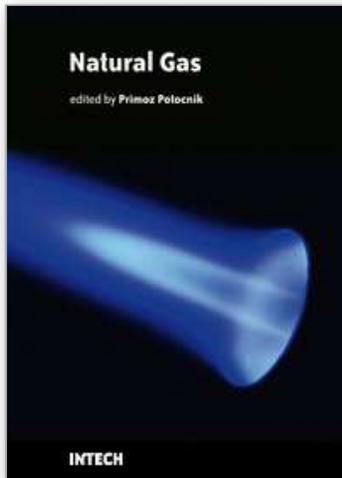
* Conversion factor is exact.

References

1. Colebrook, C.F.J. (1938), Inst. Civil Engineers, 11, p 133
2. Cullender, M.H. and R.V. Smith (1956). "Practical solution of gas flow equations for wells and pipelines with large temperature gradients". Transactions, AIME 207, pp 281-89.
3. Giles, R.V., Cheng, L. and Evert, J (2009).. Schaum's Outline Series of Fluid Mechanics and Hydraulics, McGraw Hill Book Company, New York.
4. Gopal, V.N. (1977), "Gas Z-factor Equations Developed for Computer", Oil and Gas Journal, pp 58 - 60.
5. Ikoku, C.U. (1984), Natural Gas Production Engineering, John Wiley & Sons, New York, pp. 317 - 346

6. Matter, L.G.S. Brar, and K. Aziz (1975), "Compressibility of Natural Gases", *Journal of Canadian Petroleum Technology*, pp. 77-80.
7. Ohirhian, P.U.(1993), "A set of Equations for Calculating the Gas Compressibility Factor" Paper SPE 27411, Richardson, Texas, U.S.A.
8. Ohirhian, P.U.: "Direct Calculation of the Gas Volumetric Rates", *PetEng. Calculators*, Chemical Engineering Dept. Stanford University, California, U.S.A, 2002
9. Ohirhian, P.U. and I.N. Abu (2008), "A new Correlation for the Viscosity of Natural Gas" Paper SPE 106391 USMS, Richardson, Texas, U.S.A.
10. Ohirhian, P.U. (2005) "Explicit Presentation of Colebrook's friction factor equation". *Journal of the Nigerian Association of Mathematical physics*, Vol. 9, pp 325 - 330.
11. Ohirhian, P.U. (2008). "Equations for the z-factor and compressibility of Nigerian Natural gas", *Advances in Materials and Systems Technologies*, Trans Tech Publications Ltd, Laubisrtistr. 24, Stafa - Zurich, Switzerland..
12. Ouyang, I and K. Aziz (1996) "Steady state Gas flow in Pipes", *Journal of Petroleum Science and Engineering*, No. 14, pp. 137 - 158.
13. Standing, M.B., and D.L. Katz (1942) "Density of Natural Gases", *Trans AIME* 146, pp. 140-9.
14. Standing, M.B. (1970), *Volumetric and Phase Behavior of Oil Field Hydrocarbon Systems*, La Habra, California.

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The contributions in this book present an overview of cutting edge research on natural gas which is a vital component of world's supply of energy. Natural gas is a combustible mixture of hydrocarbon gases, primarily methane but also heavier gaseous hydrocarbons such as ethane, propane and butane. Unlike other fossil fuels, natural gas is clean burning and emits lower levels of potentially harmful by-products into the air. Therefore, it is considered as one of the cleanest, safest, and most useful of all energy sources applied in variety of residential, commercial and industrial fields. The book is organized in 25 chapters that cover various aspects of natural gas research: technology, applications, forecasting, numerical simulations, transport and risk assessment.

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InTech Europe

University Campus STeP Ri
Slavka Krautzeka 83/A
51000 Rijeka, Croatia
Phone: +385 (51) 770 447
Fax: +385 (51) 686 166
www.intechopen.com

InTech China

Unit 405, Office Block, Hotel Equatorial Shanghai
No.65, Yan An Road (West), Shanghai, 200040, China
中国上海市延安西路65号上海国际贵都大饭店办公楼405单元
Phone: +86-21-62489820
Fax: +86-21-62489821

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